# Transient Reactivity of Solid Silver Acetate in Hydrogen and Oxygen by In Situ Diffuse Reflectance Infrared Fourier Transform Spectroscopy\*

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#### Abstract

The reactivity of solid silver acetate in hydrogen and oxygen has been studied by using the transient response method and the in situ diffuse reflectance infrared fourier transform spectroscopic (DRIFTS) technique to compare its nature to that of the reaction intermediates in ethylene oxidation. On the analysis of the transient response curves, solid silver acetate produced acetic acid and a small amount of carbon dioxide in a hydrogen stream, and produced CO2 and a small amount of CH3COOH in an oxygen stream. Temperature programed reaction (TPR) spectra of the two products commonly exhibited a peak temperature of 170°C in the hydrogen stream and 210°C in the oxygen stream, indicating that its reactivity in the hydrogen stream should be higher than in the oxygen stream. A possible reaction mechanism has been proposed for both streams.

A new IR cell has been developed for the in situ DRIFTS study under transient states, and it was confirmed that the response of the cell to the step change in gas composition was within two seconds. The transient responses of the characteristic absorption bands for the surface species of solid silver acetate, in the H2 stream or in the O2 stream, are in good agreement with those from the transient response method.

#### Introduction

In our previous papers1-8), it has been demonstrated that there are some stable intermediates in the complete oxidation of ethylene over a silver catalyst, when the reaction is operated at temperatures lower than 130°C. The reaction model can be visualized as

$$C_2H_4 \xrightarrow{O^-} In \text{ (intermediates)} \xrightarrow{O_2^-} CO_2, H_2O$$
 (1)

where O- and O2 are monoatomic surface oxygen species and diatomic surface oxygen species, respectively. The nature and the reactivity of one of the intermediates is quite similar to silver acetate including its infrared spectra. As our first approach to clarify the structure of the intermediate, it may reasonably be proposed that the intermediate should have a similar structure to silver acetate. From this stand point, the nature and the reactivity of solid silver acetate can be compared to those of the intermediate to relate both structures. In the present

Partly presented at the Hokkaido regional meeting of JCS in the winter period of 1984,

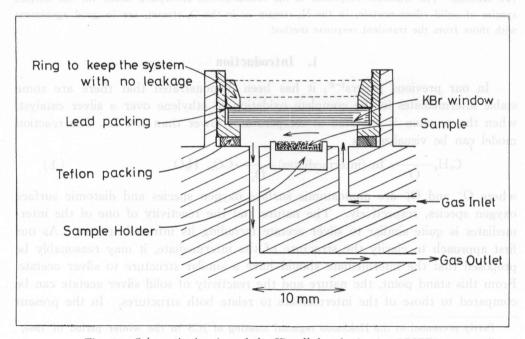
study, the characteristic reactivity of solid silver acetate has been extensively studied by using the transient response method and the diffuse reflectance infrared spectroscopic technique.

A new in situ infrared cell has been developed to accurately follow the transient response of infrared absorption bands. The new cell for the DRIFTS is extremely useful and convenient for following the transient behavior of solid surface species during the reaction with no affect from gas mixing, and to prepare the sample, which is a fine powder, it is not necessary to make pressed thin disks.

### 2. Experimental Procedure

Special grade solid silver acetate produced by Wako Pure Chemical Industries Ltd. was employed as a sample for the DRIFTS technique. Two grams of solid silver acetate were packed into four Pyrex glass tubes each of which was connected with a silicon tube, so that the sample in the reactors can be obtained for the DRIFTS technique to follow the surface structure change during the reaction. The reactors were immersed in an oil bath the temperature of which was excellently controlled within  $\pm 0.5^{\circ}$ C at the desired temperatures. The total gas flow rate was 80 cc(NTP)/min. For the transient response method, a further detailed experimental procedure will be found elsewhere.9~11)

For the in situ DRIFTS technique, a new cell was developed so as not to have any effect on gas mixing in the cell. The old cell used in our previous papers 12,13) was a diffusion type, in which the gas flow passed under a sample



Schematic drawing of the IR cell for the in situ DRIFTS.

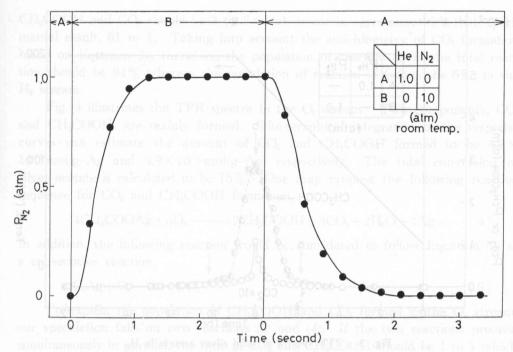


Fig. 2. Transient response of the IR cell in the step change of gas composition between  $N_2$  and He.

holder and the gas contacted the sample by molecular diffusion through four holes in the sample holder. The new cell is carefully constructed so that the gas flow goes as straight as possible, and the schematic structure of the cell is presented in Fig. 1. The gas mxing effect was examined and found to be negligible by the transient response curves between N<sub>2</sub> and He gas flows, using a quadrupole type mass spectrometer to analyse N<sub>2</sub>, where the total gas flow rate was 160 cc/min. Typical response curves obtained thus are presented in Fig. 2. As can be seen from the figure, the delay of the response curves is within two seconds, indicating no gas mixing effect in the cell.

The sample for the DRIFTS technique was prepared by mixing the solid silver acetate powder (2 wt%) with KBr powder, all of which was ground into a fine powder under 400 mesh.  $0.018\,\mathrm{g}$  of the sample  $[2.3\times10^{-4}\,\mathrm{g-Ag}]$  was placed on a sample holder and the flow rate of gas was  $30\,\mathrm{cc}$  (NTP)/min.

#### 3. Experimental Results and Discussion

#### 3-1. Transient Reactivity of Solid Silver Acetate in H<sub>2</sub> and O<sub>2</sub>.

The reactivity of solid silver acetate is extensively examined in the H<sub>2</sub> and O<sub>2</sub> gas streams under elevating temperature and the response of the outlet gas flow is followed by using gas chromatographs as continuously as possible. The response curve obtained thus may be called the temperature programed reaction (TPR) spectra. Fig. 3 is the result in the H<sub>2</sub> stream. The components of the

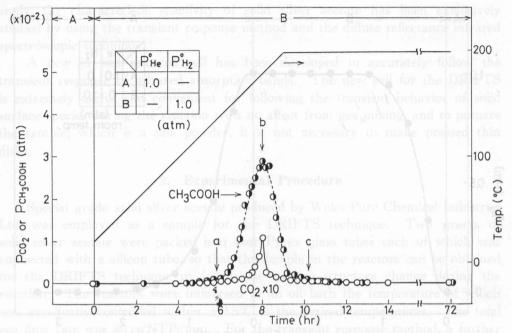


Fig. 3. TPR spectra of solid silver acetate in H<sub>2</sub>.

efluent gas stream are confirmed to be mainly acetic acid with a small amount of carbon dioxide. The graphical integration of the TPR spectra obtained gives the total amount of the components to be  $8.0(\pm0.2)\times10^{-3}\,\mathrm{mol}$  CH<sub>3</sub>COOH/g-Ag and  $0.13(\pm0.03)\times10^{-3}\,\mathrm{mol}$  CO<sub>2</sub>/g-Ag. Based on the carbon balance, the total conversion of the solid silver acetate used can be calculated to be  $90\,(\pm5)\%$  which changes depending on the degree of water content in the sample. It is difficult to remove all water in the sample because of its unstable structure at high temperatures.

From the experimental result that the color of the sample after the TPR experiment was light gray, one may speculate that the sample had been completely converted into CH<sub>3</sub>COOH and CO<sub>2</sub> to produce metallic silver. This metallic silver sample obtained thus is active for the ethylene oxidation. This is also further support for the metallic silver form, because it is experimentally confirmed that solid silver acetate is not active for the oxidation of ethylene, and the activity of silver partly containing solid silver acetate is unstable.

The mechanism for the production of acetic acid in H<sub>2</sub> may be proposed as follows,

$$2CH_3COOAg + H_2(g) \longrightarrow 2CH_3COOH(g) + 2Ag$$

For the mechanism for CO<sub>2</sub> formation, the following equation has been well known<sup>14~18)</sup>

$$4CH_3COOAg \longrightarrow 3CH_3COOH + CO_2 + C + 4Ag$$
 (3)

If Equation (3) proceeds in advantage rather than Equation (2), the ratio of

CH<sub>3</sub>COOH and CO<sub>2</sub> should be 3 to 1 which is not in agreement with the experimental result, 61 to 1. Taking into account the stoichiometry of CO<sub>2</sub> formation based on Equation (3), therefore, the population of reaction (2) in the total reaction should be 94% whereas the population of reaction (3) should be 6%, in the H<sub>2</sub> stream.

Fig. 4 illustrates the TPR spectra in the  $O_2$  stream. Two components,  $CO_2$  and  $CH_3COOH$ , are mainly formed. The graphical integration of the response curves can estimate the amount of  $CO_2$  and  $CH_3COOH$  formed to be  $4.2 \times 10^{-3} \, \text{mol/g-Ag}$  and  $4.9 \times 10^{-3} \, \text{mol/g-Ag}$ , respectively. The total conversion of silver acetate is calculated to be 75%. One may propose the following reaction sequence for  $CO_2$  and  $CH_3COOH$  formation,

$$4CH3COOAg + 3O2 \longrightarrow 2CH3COOH + 4CO2 + 2H2O + 4Ag$$
 (4)

In addition, the following reaction would be considered to follow Equation (3) as a consecutive reaction,

$$C.Ag + O_2 \longrightarrow CO_2$$
 (5)

To explain the population of CH<sub>3</sub>COOH and CO<sub>2</sub> formed in the O<sub>2</sub> stream, our speculation falls on two reactions (3) and (4). If the two reactions proceed simultaneously in parallel, the ratio of CO<sub>2</sub> and CH<sub>3</sub>COOH should be 1 to 1 which is very close to the experimental result, 1 to 1.2. This result strongly suggests that reactions (3) and (4) will proceed in parallel with the population of 1 to 1. The color of the sample after the TPR experiment in the O<sub>2</sub> stream is dark

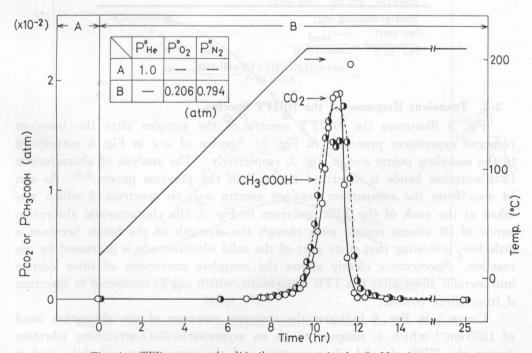


Fig. 4. TPR spectra of solid silver acetate in the O<sub>2</sub>-N<sub>2</sub> mixture.

gray. From this evidence one could speculate that some of the carbon in Equation (3) resides in the sample. This is the reason why the total conversion of silver acetate is 75% lower than that in  $H_2$ .

Comparing Figs. 3 and 4, one can see that the peak temperature of the TPR spectrum in  $H_2$  is lower than that in  $O_2$ . In addition, the starting temperature of reaction with the gaseous components is also lower than that in  $O_2$ . These results strongly support our speculation that the reactivity of silver acetate with  $H_2$  is higher than with  $O_2$ . The results are summarized in Table 1. Since solid silver acetate is less active in  $O_2$  than in  $H_2$ , reaction (4) needs higher activation energy than reaction (2). Reaction (3) in  $O_2$  should partly proceed in advantage compared to that in  $H_2$ .

Table 1. Graphical Analysis of TPR spectra in the H<sub>2</sub> or O<sub>2</sub> gas stream

	$H_2$	O <sub>2</sub> 13891
Peak Temp. (°C)	190	210
CH <sub>3</sub> COOH (×10 <sup>-3</sup> )	7.9	077 10 4.9 8
CO <sub>2</sub> (×10 <sup>-3</sup> )	0.13	4.2
conversion	0.96	0.75

 $(mol \cdot products/g-Ag)$   $conversion = \frac{total}{theoritical}$   $mol \cdot CH_3COOH + 1/2 mol \cdot CO_2$ 

 $=\frac{\text{mol}\cdot\text{CH}_3\text{COOH}+1/2\text{ mol}\cdot\text{CO}_2}{9.27\times10^{-3}}$ 

## 3-2. Transient Response of the DRIFT Spectra.

Fig. 5 illustrates the DRIFT spectra of the samples after the transient response experiment presented in Fig. 3. Spectra of a-c in Fig. 5 correspond to the sampling points a-c in Fig. 3, respectively. The analysis of characteristic IR absorption bands is described in detail in the previous papers. <sup>12,13)</sup> As can be seen from the comparison between spectra a-c, on spectrum b which was taken at the peak of the TPR spectrum in Fig. 3, the characteristic absorption bands of IR almost remain even though the strength of the bands becomes a little low, indicating that some part of the solid silver acetate is decreased by the reaction. Spectrum c clearly shows the complete conversion of silver acetate into metallic silver after the TPR experiment, which can be compared to spectrum c from silver powder.

Curve 1 in Fig. 6 indicates the transient response of the absorption band of 1575 cm<sup>-1</sup> which is assigned to be an asymmetric C-O stretching vibration during the TPR of solid silver acetate, and the temperature schedule used is

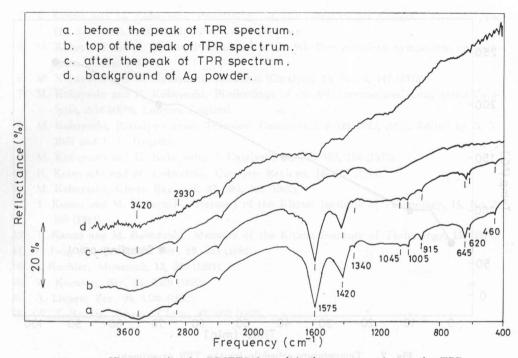


Fig. 5. IR spectra by the DRIFTS for solid silver acetate during the TPR in  $H_2$ . a, b, and c respectively correspond to a-c in Fig. 3.

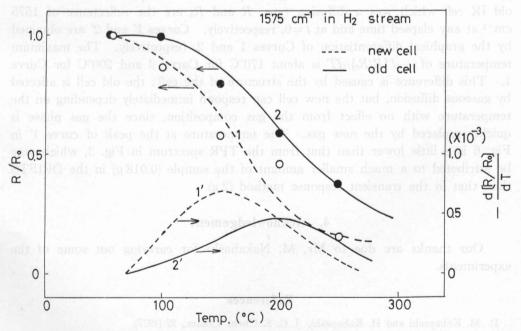


Fig. 6. Comparison of the transient response between the new IR cell and the old IR cell.

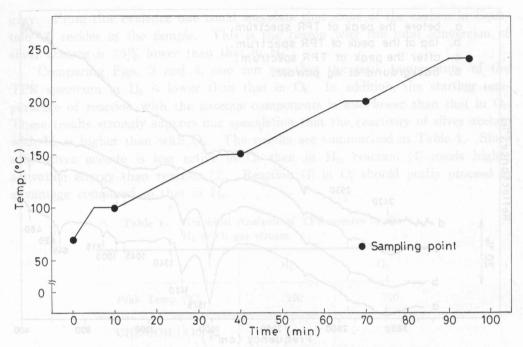


Fig. 7. Temperature schedule for the TPR experiment.

presented in Fig. 7. Curve 2 in Fig. 6 represents the response curve from the old IR cell which was a diffusion type. R and  $R_0$  are the reflectance of 1575 cm<sup>-1</sup> at any elapsed time and at t=0, respectively. Curves 1' and 2' are obtained by the graphical differentiation of Curves 1 and 2, respectively. The maximum temperature of  $-d \left[ R/R_0 \right]/dT$  is about 170°C for Curve 2 and 200°C for Curve 1. This difference is caused by the structure of the cell; the old cell is affected by gaseous diffusion, but the new cell can respond immediately depending on the temperature with no effect from the gas composition, since the gas phase is quickly replaced by the new gas. The temperature at the peak of curve 1' in Fig. 6 is a little lower than that from the TPR spectrum in Fig. 3, which may be attributed to a much smaller amount of the sample (0.018 g) in the DRIFTS than that in the transient response method (2 g).

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